

1.0

Main Investigation

- Why decentralized high recovery rate solar driven plants for brackish groundwater (GW) extraction and desalination could be beneficial to Egypt?
- Is it more economical to use PV instead of diesel generators to drive the reverse osmosis (RO) plant?
- Is there an economic advantage of replacing PV modules with Photovoltaic thermal (PVT) collectors to drive the RO plant?
- Is it feasible to use a membrane distillation (MD) process to enhance the recovery rate of the RO plant?



Energy and water availability in Egypt



Limited Fossil Fuel Resources

Egypt is a net oil importer



Egypt Total Oil Production and Consumption from 2000 to 2011

Source: U.S. Energy Information Administration (2013)

 Current natural gas reserves could be exhausted by 2028



Egypt experienced severe shortages in electricity during summer peak hours since 2010!





Water Status in Egypt: Water Sources



- Nile Water
- Nile Water Re-use
- Groundwater Extraction (Rainfall + Fossil)
- Treated Waste Water
- Seawater Desalination



Egypt is on the verge of becoming an absolutely water scarce country!





Foreseen Reduction in Nile Water Availability

- Nile water is shared with 9 other countries
- 85% of Nile water originates from the Blue Nile in Ethiopia
- Ethiopia is building a huge dam with 74 billion cubic meter of storage





Options: Groundwater extraction and Seawater desalination

- Seawater \rightarrow Essentially infinite
- Groundwater \rightarrow Limited availability



Potential Benefits to GW Extraction?





Centralisation vs. Decentralisation

- Centralised development described as unsustainable and promoting inequity (Schumacher, 1974)
- Decentralized communities require decentralized small scale infrastructure which can be easily financed
- Decentralized communities increases the resiliency of the population particularly when the workplace is in the area where people are living and where local skills can be exploited



Decentralized agricultural communities with local access to water from the ground and energy from the sun

- Shortages in water and energy availability
- 1/3 of the workforce are in the agriculture sector and mostly concentrated in rural areas where poverty rates are the highest
- Government plans to gradually remove current subsidies on food and energy
- Farmers are losing their jobs due to land degradation caused by urban encroachment



Huge Solar Resources



Africa Flat Plate Tilted at Latitude Annual Solar Irradiance (kWh/m²/day) Source: (Solar and Wind Energy Resource Assessment (SWERA, 2005)



Ground water availability in Egypt

- Where can groundwater be found?
- Is the groundwater suitable for drinking and irrigation?
- What is the aquifers' potential for sustainable development?











Challenges!

- Brackish GW definition (1,000-10,000 mg/l)
- Drinking water → Salinity <1,000 mg/l</p>



Desalination required!



Challenges!

Energy intensive and expensive process
 →Energy and cost reduction required



 Brine disposal and limited groundwater availability → High recovery rate desalination required

High recovery rate solar driven plants for brackish ground water extraction and desalination



Solar Driven Desalination





School of Photovoltaic and Renewable Energy Engineering

Most Suitable Solar Technology





Solar Driven Desalination





School of Photovoltaic and Renewable Energy Engineering

Suitability of RO for Decentralized Applications

- Lowest energy demand particularly with BW
- Lowest LCOW
- Most widely used
- Local experience
- Modularity



RO Process Description



Spiral wound RO membrane (Brennan, 2001)



Techno-Economic Feasibility of High RR PV-RO Plants

- What is the maximum attainable recovery rate?
- Is it more economical to use PV instead of diesel generators to drive the RO plant?



PV-RO Plant Configuration



- Simulation carried out using PVSYST and ROSA
- PV-RO plant designed to operate only during daytime and for 24 hours



Maximum Attainable RR



75 to 90% RR with the typical brackish GW composition found in Egypt with simple pre-treatment requirements



Economic Feasibility: Diesel Generators vs. PV

Day only operation





Economic Feasibility: Diesel Generators vs. PV



RO plant to operate for 24 hours!



Estimated LCOW of PV-RO Plants in Egypt



- LCOW: 0.7 USD/m³ to 1.65 \$US/m³ in most locations
- Current Water Prices: 0.03 to 0.34 \$US/m³ X
- LCOW Seawater PV-RO: 2 to 3 \$US/m³



SW Desalination vs. BW Extraction and Desalination: Energy Requirements



- Low Irrad. Zone/Unconfined Aquifer (10 m)
- High Irrad. Zone/ Confined Nubian Aquifer in Eastern Desert and Western Desert (20 m)
- High Irrad. Zone/ Unconfined Aquifer (50 m)
- Low Irrad. Zone/Unconfined Aquifer (50 m)
- High Irrad. Zone/ Confined Nubian Aquifer in the Sinai Peninsula (200 m)



PV-RO can be only described as cost competitive with DG-RO

 7 to 16% higher LCOW with the typical composition, and expected range of GW depths and solar irradiance found in Egypt

Is there a possibility to reduce the LCOW of the PV-RO Plant?



Sensitivity Analysis





- After reducing the nominal interest rate from 13 to 9%
 PV-RO LCOW is only 2 to 5% higher than that of DG-RO
- Reducing battery costs from 200 to 100 \$US/kWh makes a PV-RO clearly more economical





Is there any other possibility to reduce the LCOW of a PV-RO plant?



What about coupling the RO plant with PVT collectors?

A Double Benefit!

- Potential decrease in the array size through cooling the PV cells using the pumped GW
- Reducing the energy consumption of the RO plant through heating the feed water

 \rightarrow Lowers water viscosity \rightarrow makes it easier for water molecules to cross the membrane

 \rightarrow Less salt rejection



Effect of Water Temperature on the RO Plant Power Consumption



12 to 30% reduction in the power consumption by heating the water to 40°C without compromising the permeate water quality


There is a "catch", however!

- RO modules have to operate outside the recommended operating parameters
- In some designs the maximum recommended permeate flow rate was exceeded by 58%
- A properly designed RO plant results in no energy savings





PVT-RO Plant Configuration



- Yearly simulation performed using TRNSYS
- Used a more accurate PVT model developed by Bilbao and Sproul (2012)



Results



School of Photovoltaic and Renewable Energy Engineering

PV-RO vs. PVT-RO: Increase in the annual PV yield



A modest increase in the annual energy yield ranging from approximately 3.6% to less than 6.7%



PV-RO vs. PVT-RO: Reduction in RO Plant Annual Energy Requirements



A modest reduction in the RO plant energy requirements ranging from approximately 3.4% to less than 6.6%



Economic Feasibility of PVT-RO



Even with the best possible cases, there is no economic advantage of replacing PV modules with PVT collectors



Reasons for the unfeasibility of PVT-RO

- The low capacity factor of the PVT collectors and the variability of solar irradiance → a percentage reduction in the RO plant annual energy consumption not exceeding 6.6% in comparison to values up to approximately 30% if the water was continuously heated to 40°C
- The operating temperature limitation of the RO membranes
- Using PVT collectors mainly resulted in reducing the required PV cell area while had a negligible impact on the battery bank supacity required
- Even a fetoassuming that replacing the PV Modules with PVT collectors will produces with PVT collectors will produce with additional costs, the decrease in the transmission of the produce of the second costs. The decrease is a second cost of the second cost

Hours



Challenges!

- Brackish GW Definition (1,000-10,000 mg/l)
- Drinking Water → Salinity <1,000 mg/I</p>
- Energy Intensive Process
- Brine disposal and water utilization
 - → High recovery rate desalination required
 - → Recovery rate ceiling of the RO plant ranged from 80 to 90% (No scaling limitations)



Is there a possibility to further increase the recovery rate to values beyond those achieved by an RO plant?



Possible using a thermal desalination process

- No feed pressure limitations
- Production less affected by feed water salinity
- Increasing salinity from 35,000 to 50,000 mg/l
 - \rightarrow 7% increase in MD energy
 - → at least 43% increase in RO energy consumption



Using a Membrane Distillation Process?

- Robust and simple to use
- Modular
- Needs a low grade source of energy
- Low pressure operation
- Large potential for improvement



MD Process Description



- 1- Hot feed water flow
- 3- Water vapour molecules
- 5- Vapour-Liquid Interface

- 2- Cold water flow mixed with distillate
- 4- Hydrophobic membrane material
- 6- Membrane Pore



The hybrid RO/MD concept was investigated before

- Only for seawater applications
- Based on the performance of a lab scale module (Drioli et al., 1999)
- Unrealistic specific heat consumption
- High flux at 320 g/l brine concentration \rightarrow unrealistic

New feasibility study is needed with realistic data from a full scale module!



PGMD Module





Source: (Winter et al., 2011)



School of Photovoltaic and Renewable Energy Engineering

PGMD Module Modelling





The model gave good agreement with the experimental results with a mean deviation of less than 3.35% from experimental values





Hybrid RO/MD Plant Configuration





Solar Driven MD Plant Configuration



Modified after (Schwantes et al., 2013)



Solar driven MD plant modelled and optimized using TRNSYS





What is the maximum attainable recovery rate from a hybrid RO/MD plant?



Hybrid RO/MD Plant Maximum Attainable RR



- Max RO RR (Design Limited) at 20-40°C
- Max RR pH=6 Low Scaling Potential GW
- Max RR pH=6 High Scaling Potential GW
- × Max RR pH=6 Typical Composition GW

RR enhancement only possible with additional pretreatment requirements
Up to 98% RR was obtained experimentally (Martinetti et al., 2009)



Hybrid RO/MD Plant Maximum Attainable RR



- Max RO RR (Design Limited) at 20-40°C
- Expected Max. Attainable RR (Simple Pre-treatment)
- Actual . Attainable RR (Simple Pre-treatment)
- × Actual Max. Attainable RR (Further Pre-treatment)
- No more than 10% enhancement in the RR was possible even after the assumption that further pretreatment is used (i.e. 250 g/kg brine concentration possible)



Cooling tower evaporation losses have a significant impact on the max. attainable recovery rate!

- The MD module has very low RR (<5%)</p>
- Large brine needs to be recirculated





Can higher recovery rates be achieved with enhanced MD configurations?



- MEMSYS Module:
 - \rightarrow VMD process
 - \rightarrow 9 folds the recovery rate of PGMD module



 The increase in the MD module recovery rate was totally offset by the large cooling flow rate which increased the evaporation losses in the cooling tower



Even with such small enhancement in the recovery rate:

Is it economically feasible to use a hybrid plant?



School of Photovoltaic and Renewable Energy Engineering

Solar driven MD plant performance





Solar Driven MD Plant Configuration



Modified after (Schwantes et al., 2013)



Using a hybrid plant resulted in a significant increase in the LCOW

Confined Nubian Aquifer in the Sinai Peninsula (200 m) 10 g/l GW

Unconfined Aquifer (50 m) 10 g/l GW

Confined Nubian Aquifer in Eastern Desert and Western Desert (20 m) 10 g/I GW

> Confined Nubian Aquifer in the Sinai Peninsula (200 m) 2 g/I GW

Unconfined Aquifer (50 m) 2 g/l GW

Confined Nubian Aquifer in Eastern Desert and Western Desert (20 m) 2 g/I GW

Hybrid PlantRO Plant





Why so expensive?



School of Photovoltaic and Renewable Energy Engineering

MD Plant Cost Breakdown



■ FPC Indirect Costs MD Modules Heat Exchangers Installation Heat Storge Tank PV System Costs Instrumentation FPC Racking Module Housing

Piping & Tanks

Conclusion: The low flux and high SHC of the PGMD module are the main reasons behind the high LCOW of the MD plant which ranged from 40.5 to 50.5 \$US/m³



Under what conditions can a hybrid RO/MD plant become more economical?



School of Photovoltaic and Renewable Energy Engineering



LCOW (USD/m³)



Using a hybrid Plant to enhance the recovery rate of BW PV-RO plant could be more economical under the following conditions:

- The MD plant needs to be driven using waste heat from a renewable energy source such as CPV or CSP plant
- The MD module should experience at least 4 folds reduction in its heat consumption or 2 folds increase in its flux and 2 folds reduction in its heat consumption
- MD modules costs needs to drop to 100 \$US/m²

Only 26 to 47% increase in the LCOW is expected in this case for brackish water applications



Is it worth to combine a thermal process with an RO plant to increase the RR?

- RR's ranging from 75 to 90% were already attainable from the RO plant
- Higher RR requires additional pretreatment requirements
- Using other thermal processes is likely to have the same limitations
- Salt retrieval?



Conclusion

- Why decentralized high recovery rate solar driven plants for brackish groundwater (GW) extraction and desalination could be beneficial to Egypt?
- Is it more economical to use PV instead of diesel generators to drive the reverse osmosis (RO) plant?
- Is there an economic advantage of replacing PV modules with Photovoltaic thermal (PVT) collectors to drive the RO plant?
- Is it feasible to use a membrane distillation (MD) process to enhance the recovery rate of the RO plant?


Decentralized high recovery rate solar driven plants for brackish GW extraction and desalination are suggested to establish decentralized agricultural communities in Egypt with a degree of autonomy to increase the resiliency of a large sector of the population



- Why decentralized high recovery rate solar driven plants for brackish groundwater (GW) extraction and desalination could be beneficial to Egypt?
- Is it more economical to use PV instead of diesel generators to drive the reverse osmosis (RO) plant?
- Is there an economic advantage of replacing PV modules with Photovoltaic thermal (PVT) collectors to drive the RO plant?
- Is it feasible to use a membrane distillation (MD) process to enhance the recovery rate of the RO plant?



 A PV driven RO plant operating for 24 hours is cost competitive with a DG-RO if the current subsidies on diesel are removed and becomes more economical if the battery costs dropped to 100 \$US/kWh

The LCOW and the SEC of PV-RO plants used to extract and desalinate brackish water were also found to be lower than those of a SW PV-RO plant



- Why decentralized high recovery rate solar driven plants for brackish groundwater (GW) extraction and desalination could be beneficial to Egypt?
- Is it more economical to use PV instead of diesel generators to drive the reverse osmosis (RO) plant?
- Is there an economic advantage of replacing PV modules with Photovoltaic thermal (PVT) collectors to drive the RO plant?
- Is it feasible to use a membrane distillation (MD) process to enhance the recovery rate of the RO plant?



The Low capacity factor ,variability of solar irradiance and operating temperature limitation of the RO membranes are main barriers for PVT collectors to have any economic advantage over standard PV modules with RO applications

- Why decentralized high recovery rate solar driven plants for brackish groundwater (GW) extraction and desalination could be beneficial to Egypt?
- Is it more economical to use PV instead of diesel generators to drive the reverse osmosis (RO) plant?
- Is there an economic advantage of replacing PV modules with Photovoltaic thermal (PVT) collectors to drive the RO plant?
- Is it feasible to use a membrane distillation (MD) process to enhance the recovery rate of the RO plant?



 Less than 10% enhancement in the RR was achieved using a hybrid RO/MD plant with a corresponding significant increase in the LCOW

 The evaporation losses from the cooling tower were found to have a significant impact on the maximum attainable RR from a hybrid RO/MD plant even with enhanced MD process configurations

 For higher recovery rates to be achieved with a hybrid RO/MD plant, higher recovery rate MD modules with low cooling requirements are needed

 Hybrid RO/MD plants are likely to be only economically feasible if a source of a waste heat is available from a CPV or a CSP plant, the SHC of the process is reduced by 4 folds and the MD module costs become similar to that of an RO module



Future Work

- Dual use of CPV to generate electricity and to drive a low temperature thermal desalination process such as MD
- Battery-less PV-RO plants, is it worth it when brackish water is desalinated?
- Spiral wound vs. planar geometry assumption



References

BILBAO, J. & SPROUL, A. B. 2012, Analysis of Flat Plate Photovoltaic-Thermal (PVT) Models, World Renewable Energy Forum (WREF) Including World Renewable Energy Congress XII and Colorado Renewable Energy Society (CRES) Annual Conference, Denver, Colorado, USA.

DRIOLI, E., LAGANÀ, F., CRISCUOLI, A. & BARBIERI, G. 1999 Integrated membrane operations in desalination processes, Desalination 122, 141-145.

MARTINETTI, C. R., CHILDRESS, A. E. & CATH, T. Y. 2009 High recovery of concentrated RO brines using forward osmosis and membrane distillation, Journal of Membrane Science 331, 31-39

SCHWANTES, R., CIPOLLINA, A., GROSS, F., KOSCHIKOWSKI, J., PFEIFLE, D., ROLLETSCHEK, M. & SUBIELA, V. 2013 Membrane distillation: Solar and waste heat driven demonstration plants for desalination, Desalination 323, 93-106

SWERA 2005 Flat Plate Tilted at Latitude Annual, SWERA, accessed 7 September 2010, <u>http://swera.unep.net/typo3conf/ext/metadata_tool/archive/download/africatilt_218.pdf</u>.

U.S. ENERGY INFORMATION ADMINISTRATION 2013, Egypt, EIA, accessed 16 November 2013, http://www.eia.gov/countries/country-data.cfm?fips=EG

WATER QUALITY ASSOCIATION 2005 Osmosis Process, HM Digital, accessed 11 August 2010, http://www.tdsmeter.com/what-is?id=0013

WINTER, D., KOSCHIKOWSKI, J. & WIEGHAUS, M. 2011 Desalination using membrane distillation: Experimental studies on full scale spiral wound modules, Membrane Science 375, 104-112



Acknowledgment

I would like to thank the Fraunhofer Institute team for their valuable contribution and support



Thank you for your attention





School of Photovoltaic and Renewable Energy Engineering

Further Info Slides



School of Photovoltaic and Renewable Energy Engineering

Further RR Limitations when driven by solar energy



Collector Area to MD Modules Ratio (m²/NMD)



Impact of PV-RO Plant Operating Hours on the LCOW



More economical to design the plant to run for 24 hours with BW applications



Two Locations: Aswan & Marsa-Matruh

→ Two extremes in solar irradiance and groundwater temperatures





School of Photovoltaic and Renewable Energy Engineering

Glazed vs. Unglazed Collectors

- Glazed Collectors: High Thermal Output/Low Electrical Output
- Unglazed Collectors: Low Thermal Output/ High Electrical Output



